

Total No. of Questions : 10]

SEAT No. :

P3249

[Total No. of Pages : 4

[5353] - 112
T.E. (Mechanical)
HEAT TRANSFER
(End Semester)
(2012 Pattern)

Time : 2½ Hours]

[Max. Marks : 70

Instructions to the candidates:

- 1) *Solve Q.1 or Q.2. Q.3 or Q.4, Q5. or Q.6, Q.7 or Q.8, Q.9 or Q.10.*
- 2) *Draw Neat diagrams wherever necessary.*
- 3) *Use of scientific calculator is allowed.*
- 4) *Assume suitable data where ever necessary.*
- 3) *Figures to the right indicate full marks.*

Q1) a) A chemical reactor vessel of spherical shape of outside radius of 0.5 m has to loose heat at the rate of 650w in order to maintain the temperature of the chemical. The surface temperature of vessel is 125°C. The surrounding is at 113°C. If the heat loss is by both convection and radiation, determine the value of convective heat transfer coefficient required. Assume $\epsilon = 0.55$ [6]

b) Derive an expression for critical radius of insulation for cylinder. [4]

OR

Q2) a) Write 3D Heat conduction equation in cartesian co-ordinates and reduce it to fouriers equation, poissons equation and laplace equation. [6]

b) What is an insulating material? Give four examples of insulating materials [4]

Q3) a) Consider a solid sphere of radius 2cm, in which internal energy is generated uniformly at constant rate of $2 \times 10^8 \text{ w/m}^3$ conductivity of cylinder material is 30 w/mk and its outer surface is maintained at 100°C. Calculate centre temperature and heat flux at the surface of the sphere. Derive the expressions you use. [6]

b) Write a note on temperature boundary condition and heat flux boundary condition. [4]

P.T.O.

OR

Q4) a) A cylindrical fin is 3mm in diameter and 3cm long. Calculate the value of the temperature at fin tip if the fin is made of. [6]

i) Copper ($k = 350 \text{ W/mK}$) and

ii) Teflon ($k = 0.35 \text{ W/mK}$)

Assume the heat loss from fin tip is negligible.

Take $h = 10 \text{ W/m}^2\text{K}$, $T_{\text{base}} = 120^\circ\text{C}$.

Surrounding fluid temperature is 20°C

b) Steel balls of 12mm diameter are annealed by heating to 877°C and then slowly cooling to 127°C in an environment where temperature is 52°C . The heat transfer coefficient is $20 \text{ W/m}^2\text{K}$. Calculate the time required by the balls to reach the desired temperature. Use following properties, for steel. Density = 7800 kg/m^3 , $C_p = 600 \text{ J/kg K}$, $K = 40 \text{ W/mK}$ [4]

Q5) a) Explain the following with their applicability. [8]

i) Nusselt number

ii) Grashoff's Number

iii) Rayleigh number

iv) Prandtl number

b) Liquid mercury flows at a rate of 1.6 kg/sec through a copper tube of 20 mm diameter. The mercury enters the tube at 15°C and leaves at 35°C . Calculate the tube length if the tube wall temperature is 50°C . The properties of mercury at 25°C are. [8]

$\rho = 13582 \text{ kg/m}^3$, $C_p = 140 \text{ J/kg K}$, $k = 8.69 \text{ W/mK}$, $\nu = 1.5 \times 10^{-7} \text{ m}^2/\text{s}$

$\text{Pr} = 0.0248$

Use $\text{Nu} = 7 + 0.025 (\text{Re Pr})^{0.8}$

OR

Q6) a) A rectangular plate of length 7 cm and width 4 cm is maintained at 115°C . It is exposed to still air at 25°C on both sides. Calculate convective heat transfer rate if smaller side of the plate is held vertical compare heat transfer when larger side is held vertical. [8]

Use correlation $\text{Nu} = 0.59 (\text{Gr Pr})^{0.25}$

For air, at 70°C , $k = 0.03 \text{ W/mK}$, $\text{Pr} = 0.697$;

Kinematic viscosity $\nu = 2.076 \times 10^{-6} \text{ m}^2/\text{s}$

- b) Explain the concept of thermal boundary layer. [4]
- c) Show with neat sketch direction of natural convection Fluid flow (Development of thermal boundary layer) when [4]
 - i) Plate is kept vertical and surrounding fluid temperature is higher than plate.
 - ii) Cylinder is kept vertical and surrounding fluid temperature is lower than cylinder.

Q7) a) Two large parallel planes 'A' and 'D' are maintained at temperature of 1500K and 600K respectively $\epsilon_A = 0.9$ & $\epsilon_D = 0.4$ Two radiation shields 'B' with emissivity = 0.5 and 'C' with emissivity = 0.2 are inserted in between them such that A, B, C and D are placed one after the other. Calculate. [10]

- i) Heat transfer rate without radiation shields.
- ii) Heat transfer rate with radiation shields.
- iii) Temperature attained by planes 'B' and 'C'

b) State and explain any 4 properties/ rules of radiation shape factor. [6]

OR

Q8) a) If the shape factor between two adjacent sides of rectangular room is 0.22, find the shape factor between opposite faces. [4]

b) Define radiosity and irradiation. [4]

c) i) Differentiate between filmwise and dropwise condensation. [8]

ii) Design criteria for Heat exchanger

Q9) a) Derive the expression for effectiveness of parallel flow heat exchanger by using NTU method using standard notations. [9]

b) A counter flow shell and tube type heat exchanger is used to heat water at a rate of 0.8 kg/sec from 30°C to 80°C with hot oil entering at 120°C and leaving at 85°C. Calculate the size of heat exchanger required. Overall heat transfer coefficient is 125 W/m²°C. Take specific heat for water as 4180 J/kg °C. [9]

OR

Q10)a) Hot air at 66°C is cooled up to 38°C by means of cold air entering at 15.5°C . Mass flow rates of hot and cold air are 1.25 kg/s and 1.6kg/s respectively sp. heat of hot and cold air = 1.05kJ/kg K $U = 80\text{ W/m}^2\text{K}$. Find the area of the heat exchanger for parallel flow configuration.

If the same exchanger is operated in counter flow mode, find the exit temperatures of both the fluids. [12]

b) Explain 'Film boiling' Phenomenon in pool boiling process and show this region on the pool boiling curve. [6]

